

## Chapter 4. The Thermodynamics of Real Systems

### 4.1 Criteria for Spontaneous Processes and for Equilibrium : The Gibbs and Helmholtz Energies

#### 1. Criteria for Spontaneous Process in Closed Systems

由  $T_{\text{surr}}dS \geq dq$  出發

$$T_{\text{surr}}dS \geq dU - dw$$

通式  $dU - dw - T_{\text{surr}}dS \leq 0$  結合第一、二定律之 criteria

(1) isolated system  $dU = dw = 0$

$$\text{故 } \Delta S_{\text{isol.}} \geq 0$$

(2) constant  $S, dw = 0$  (即: constant  $V$  for simple system)

$$(dU)_{S,V} \leq 0$$

(3) constant  $T, V$  之 simple system,  $dw = 0, T_{\text{surr}} = T$

$$dU - TdS \leq 0 \quad \text{定義 } A = U - TS, \quad d(A)_{T,V} \leq 0$$

Helmholtz Free Energy

(4) constant  $T, P$  之 simple system,  $P_{\text{ext}} = P, T_{\text{surr}} = T$

$$dU + PdV - TdS \quad \text{定義 } G = U + PV - TS, \quad d(G)_{T,P} \leq 0$$

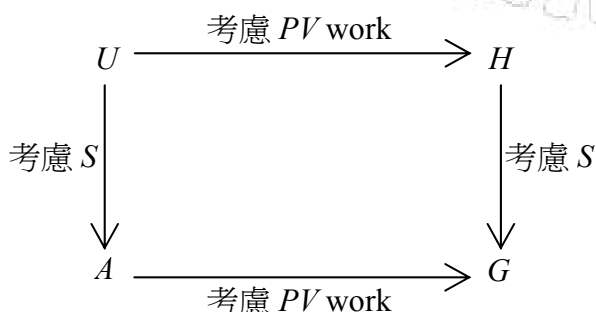
Gibbs Free Energy

$$G = H - TS = A + PV$$

$$\text{亦即: } (dS)_{U,V} \geq 0, \quad (dU)_{S,V} \leq 0, \quad (dA)_{T,V} \leq 0, \quad (dG)_{T,P} \leq 0$$

isolated system      對 simple system 而言  
(即只作  $PV$  work)

<對於  $G, A$  強調一下此時已 implicitly 考慮 surrounding 之  $\Delta S$ >



<Note>

(1)  $(\Delta G)_{T,P} \leq 0$  表示  $\Delta H - T\Delta S \leq 0$

低溫時,  $\Delta H$  重要, 所以 Berthlot 才會誤以為  $\Delta H \leq 0$  是自發反應之條件  
 高溫時,  $T\Delta S$  重要, 亦即  $\Delta S \geq 0$  決定是否自發

(2) 再強調一下, 此時已 implicitly 考慮到 surrounding

$$\begin{aligned} \text{constant } T, P \text{ 時, 由 } \Delta S_{\text{sys}} + \Delta S_{\text{surr}} &= \Delta S_{\text{sys}} + \frac{\Delta q_{\text{surr}}}{T_{\text{surr}}} = \Delta S_{\text{sys}} - \frac{\Delta q_{\text{sys}}}{T_{\text{surr}}} \\ &= \Delta S_{\text{sys}} - \frac{\Delta H_{\text{sys}}}{T} = -\frac{\Delta G_{\text{sys}}}{T} \geq 0 \end{aligned}$$

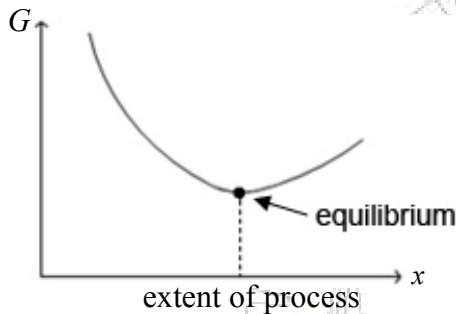
即定溫定壓下  $\Delta G \leq 0$ , 和  $\Delta S_{\text{sys}} + \Delta S_{\text{surr}} \geq 0$  意義相同

## 2. Criteria for a Closed Simple System at Equilibrium

由上知, 任何 spontaneous process 都會使  $A$  or  $G$  降低, 直至平衡 (only for simple system)

故

$(dG)_{T,P} = 0$	$(dA)_{T,V} = 0$
$(d^2G)_{T,P} \geq 0$	$(d^2A)_{T,V} \geq 0$



§ 以  $G$  為例, 在定溫下水汽化為水蒸氣

$$\Delta G = \Delta H - T\Delta S = 0 \text{ at equilibrium}$$

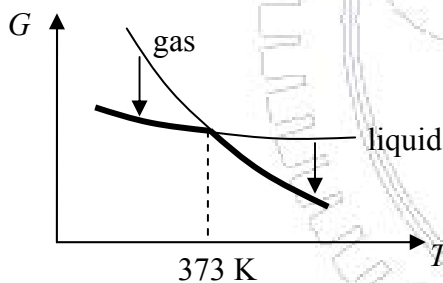
水汽化,  $\Delta H$  及  $\Delta S$  均為正

$$373 \text{ K 時, } \Delta H = T\Delta S$$

大於 373 K 時, 第二項 ( $T\Delta S$ ) 變大,  $\Delta G < 0$ , 汽化是 spontaneous, 即 gas 是 equilibrium state

小於 373 K 時, 第一項 ( $\Delta H$ ) 較大,  $\Delta G > 0$ , 即汽化不會自動發生

但  $\Delta G$  (condensation)  $< 0$ , 液化是自發的, 即: liquid 是 equilibrium state



## 3. Maximum Work <A 及 G 之意義>

$$dU - dw - T_{\text{surr}} dS \leq 0$$

(1) constant  $T$  時,  $dU - TdS - dw \leq 0$ , 即  $(dA)_T \leq dw$

或  $w_{\text{surr}} \leq -(\Delta A)$ , 等號在平衡時成立

Maximum work can be done on the surrounding in an isothermal process.

☆ 只是給 limit, reversible 步驟時是 max, 否則  $w_{\text{surr}}$  較小

$\Delta A$  是不變的 (不管是否 reversible),  $w_{\text{surr}}$  則會變

(2) 將 work 分為  $PV$  work 及其他 work (如: 電功, 表面張力)

$$dw = -P_{\text{ext}} dV + dw_{\text{net}}$$

↑                      ↙

compression work    net work

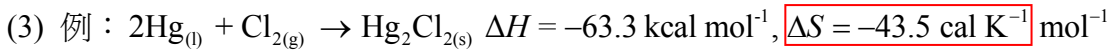
通式改爲  $dU - T_{\text{surr}} dS + P_{\text{ext}} dV - dw_{\text{net}} \leq 0$

constant  $T, P$  時,  $dU - TdS + PdV \leq dw_{\text{net}}$

即  $(dG)_{T, P} \leq dw_{\text{net}}$ , 或  $w_{\text{surr (net)}} \leq -(\Delta G)$

Maximum non-PV work at constant  $T, P$

$(dG)_{T, P} = dw_{\text{net}}$  at equilibrium



①  $\Delta G = \Delta H - T\Delta S = -63.3 - 298 \times (-43.5) \times 10^{-3}$

$= -50.4 \text{ kcal mol}^{-1}$  ( $\Delta S$  之正負決定  $\Delta H$  較  $\Delta G$  爲大或小)

② constant  $P$  下作反應, 則放熱  $63.3 \text{ kcal mol}^{-1}$  ( $-\Delta H$ )

③ 用 reversible electrochemical cell, 則放熱較小 (部分能量變爲電功)

$\Delta q_{\text{surr}} = (\Delta S_{\text{surr}})T_{\text{surr}} = (-\Delta S_{\text{sys}})T = 43.5 \times 298 \times 10^{-3} = 12.9 \text{ kcal mol}^{-1}$

其中  $\Delta S_{\text{surr}} = -\Delta S_{\text{sys}}$ , 而所作電功  $= w_{\text{net}} = 50.4 \text{ kcal mol}^{-1}$  ( $-\Delta G$ )

④ 在②之情形,  $\Delta S_{\text{surr}} = \frac{63.3 \times 10^3}{298} = 212.4 \text{ cal K}^{-1} \text{ mol}^{-1}$ ,  $\Delta S_{\text{sys}} + \Delta S_{\text{surr}} > 0$ , 自動發生

⑤ 如 cell 不是 reversible, 則所作電功較少, 放熱較多

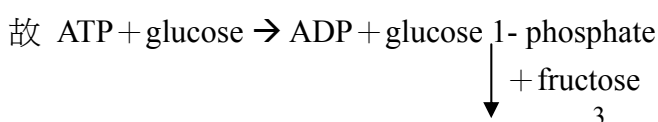
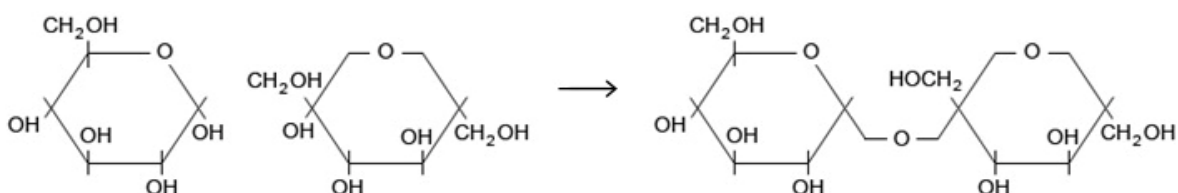
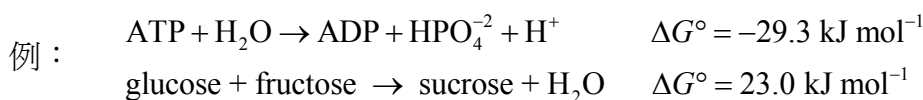
( $TdS = -12.9 \text{ kcal mol}^{-1} > dq$ , 放熱爲  $-dq > 12.9 \text{ kcal mol}^{-1}$ )

#### 4. 生物化學之熱力學

$$\begin{cases} \Delta G < 0 & \text{exergonic reaction} \\ \Delta G > 0 & \text{endergonic reaction} \end{cases}$$

在生命體中, 有很多反應是  $\Delta G > 0$  的,

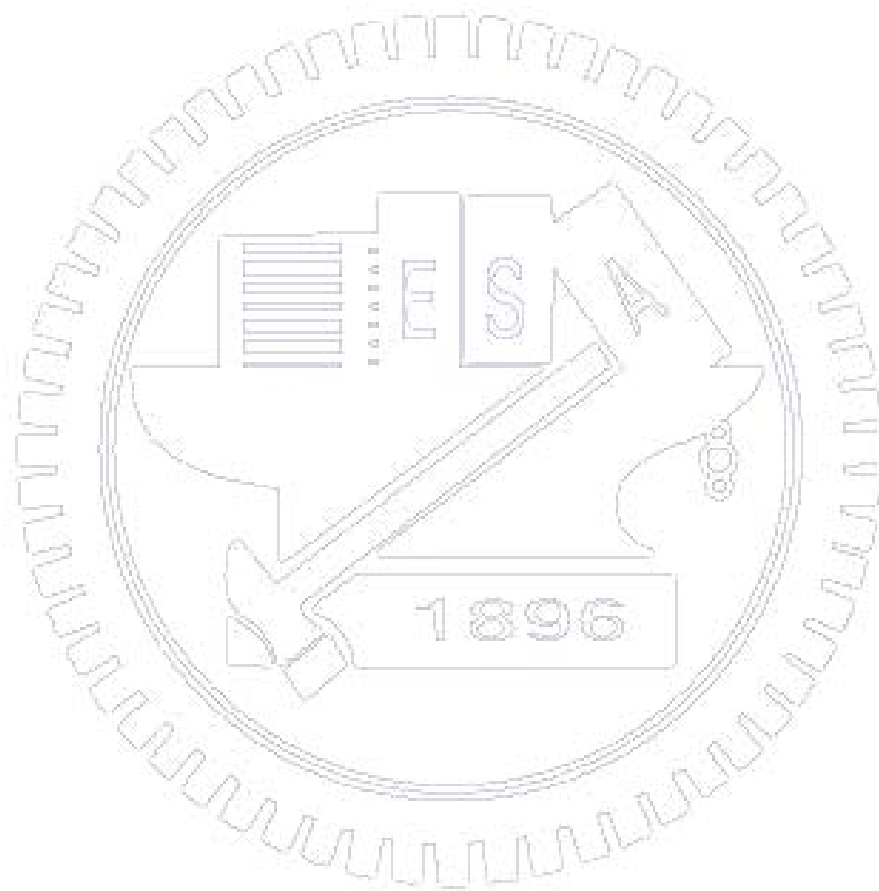
但可以靠一些  $\Delta G < 0$  之反應與之 couple, 使之  $\Delta G_{\text{total}} < 0$



sucrose

即：ATP + glucose + fructose  $\rightarrow$  sucrose + ADP

$\Delta G = 23.0 - 29.3 = -6.3 \text{ kJ mol}^{-1}$  可發生



## 4.2 Fundamental Relations for Closed Simple Systems

Simple (只有  $PdV$ ), closed system, reversible process

$$P_{\text{ext}} = P, T_{\text{surr}} = T, dq \xrightarrow{\text{才可}} TdS$$

$$\begin{aligned} dU &= dq_{\text{rev}} - PdV \\ &= TdS - PdV \end{aligned}$$

$$dU = TdS - PdV$$

$$dH = TdS + VdP$$

$$dA = -SdT - PdV$$

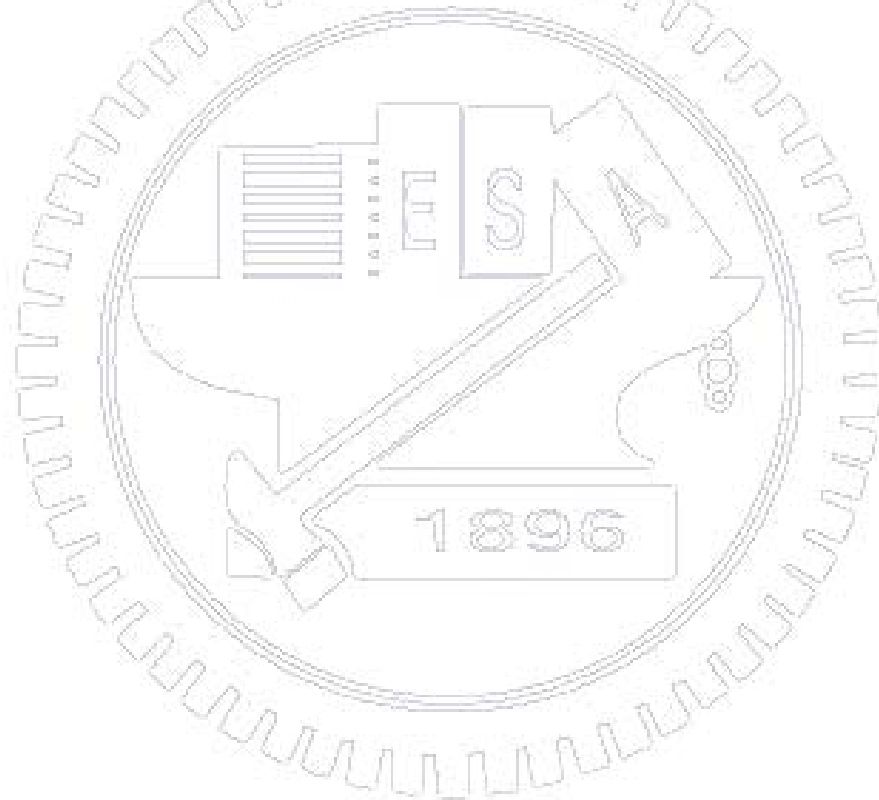
$$dG = -SdT + VdP$$

$$\text{即：} \left( \frac{\partial U}{\partial S} \right)_V = T, \left( \frac{\partial U}{\partial V} \right)_S = -P$$

$$\left( \frac{\partial H}{\partial S} \right)_P = T, \left( \frac{\partial H}{\partial P} \right)_S = V$$

$$\left( \frac{\partial A}{\partial T} \right)_V = -S, \left( \frac{\partial A}{\partial V} \right)_T = -P$$

$$\left( \frac{\partial G}{\partial T} \right)_P = -S, \left( \frac{\partial G}{\partial P} \right)_T = V$$



### 4.3 Additional Useful Thermodynamic Identities

#### 1. Maxwell Relations:

由  $\left(\frac{\partial^2 U}{\partial S \partial V}\right) = \left(\frac{\partial^2 U}{\partial V \partial S}\right)$  知  $-\left(\frac{\partial P}{\partial S}\right)_V = \left(\frac{\partial T}{\partial V}\right)_S$  或  $-\left(\frac{\partial S}{\partial P}\right)_V = \left(\frac{\partial V}{\partial T}\right)_S$   
即U是exact

同理  $\left(\frac{\partial T}{\partial P}\right)_S = \left(\frac{\partial V}{\partial S}\right)_P$  或  $\left(\frac{\partial P}{\partial T}\right)_S = \left(\frac{\partial S}{\partial V}\right)_P$

$\left(\frac{\partial S}{\partial V}\right)_T = \left(\frac{\partial P}{\partial T}\right)_V$  或  $\left(\frac{\partial V}{\partial S}\right)_T = \left(\frac{\partial T}{\partial P}\right)_V \xrightarrow{\text{回顧}} dS = \frac{C_V}{T} dT + \left(\frac{\partial P}{\partial T}\right)_V dV$

$\left(\frac{\partial S}{\partial P}\right)_T = -\left(\frac{\partial V}{\partial T}\right)_P$  或  $\left(\frac{\partial P}{\partial S}\right)_T = -\left(\frac{\partial T}{\partial V}\right)_P \xrightarrow{\text{回顧}} dS = \frac{C_P}{T} - \left(\frac{\partial V}{\partial T}\right)_P dP$

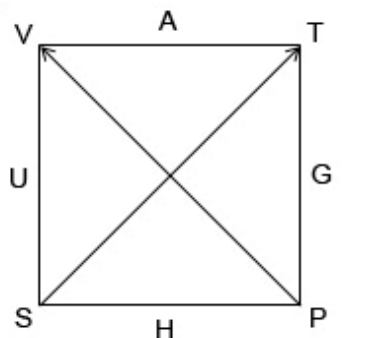
每一式子，如： $\left(\frac{\partial P}{\partial T}\right)_S = \left(\frac{\partial S}{\partial V}\right)_P$ ， $P, V$ 和 $T, S$ 成對存在，

而"下面"的constant either 是 reverse, 如： $S, V \rightarrow V, S$  [例： $-\left(\frac{\partial P}{\partial S}\right)_V = \left(\frac{\partial T}{\partial V}\right)_S$ ]

或是  $T, S \rightarrow V, P$  [例： $\left(\frac{\partial P}{\partial T}\right)_S = \left(\frac{\partial S}{\partial V}\right)_P$ ]

(只是爲了那些不求甚解的同學，其實真正懂了，根本不必如此背)

<記法>



逆時針：

“A Very Ugly Shrimp Has Pretty Good Taste”

順時針：

“The Green Plant Has Strong UV Absorption”

或

交大應化系是 “A Terribly Good Place Having Such Unusual Values”

取每一字之第一字母即依序爲左圖之各 state parameter

extensive                      intensive

( ↗ 所指即爲負值 )

由此圖可導出 ① 基本式，如

$dU = TdS - PdV$  (看最左邊一行， $U$ 是 function of  $S$  和  $V$ ，箭頭射向  $V$ ，故  $PdV$  爲負號)

② Maxwell relations：如  $-\left(\frac{\partial P}{\partial S}\right)_V = \left(\frac{\partial T}{\partial V}\right)_S$

將圖中間畫一根垂直切線，再逆時針轉  $90^\circ$ ，正負號由兩個箭頭方向是否一致決定

#### 2. 補證明

①  $\left(\frac{\partial U}{\partial V}\right)_T = \left(\frac{\partial U}{\partial V}\right)_S + \left(\frac{\partial U}{\partial S}\right)_V \left(\frac{\partial S}{\partial V}\right)_T = -P + T \left(\frac{\partial S}{\partial V}\right)_T = T \left(\frac{\partial P}{\partial T}\right)_V - P$

②  $\left(\frac{\partial H}{\partial P}\right)_T = -T \left(\frac{\partial S}{\partial P}\right)_T + V \left(\frac{\partial P}{\partial P}\right)_T = -T \left(\frac{\partial V}{\partial T}\right)_P + V$

③  $C_P - C_V = \alpha^2 VT / \kappa_T$ ，如講義第二章所列

3. 將 partial derivative 表為  $\alpha$ ,  $\kappa_T$ ,  $C_p$ ,  $P$ ,  $V$ ,  $T$  之系統性方法：

(1) 如有  $U, A, H, G$  將其變為“分子”(偏微分之上方)再消去

$$\text{如：} \left( \frac{\partial U}{\partial T} \right)_V = C_V, \left( \frac{\partial H}{\partial T} \right)_P = C_P$$

有時要彼此互變：看“分母”及“constant”，兩個 parameter 最適用於何 state function 為“分子”，

如： $T, P$  適用於  $G$  之微分

$$\text{故} \left( \frac{\partial H}{\partial T} \right)_P \rightarrow \left( \frac{\partial G}{\partial T} \right)_P + \left( \frac{\partial TS}{\partial T} \right)_P = -S + S + T \left( \frac{\partial S}{\partial T} \right)_P = T \left( \frac{\partial S}{\partial T} \right)_P$$

(2) 如有  $S$ , 則 ① 用 Maxwell relation 消去

$$\text{② 用} \left( \frac{\partial S}{\partial T} \right)_V = \frac{C_V}{T}, \left( \frac{\partial S}{\partial T} \right)_P = \frac{C_P}{T}, \text{ 因為} \left( \frac{\partial S}{\partial T} \right)_V = \left( \frac{\partial S}{\partial U} \right)_V \left( \frac{\partial U}{\partial T} \right)_V = \frac{1}{T} C_V$$

(3) 如有  $V$ , 則變為  $\alpha \left[ = \frac{1}{V} \left( \frac{\partial V}{\partial T} \right)_P \right]$ , 及  $\kappa_T \left[ = -\frac{1}{V} \left( \frac{\partial V}{\partial P} \right)_T \right]$

(4) 如有  $C_V$ , 則利用  $C_P - C_V = \alpha^2 VT / \kappa_T$

$$\langle \text{例 1} \rangle \mu_{JT} = \left( \frac{\partial T}{\partial P} \right)_H = \frac{-\left( \frac{\partial H}{\partial P} \right)_T}{\left( \frac{\partial H}{\partial T} \right)_P} = -\frac{\left( \frac{\partial G}{\partial P} \right)_T + T \left( \frac{\partial S}{\partial P} \right)_T}{C_P} = -\frac{V - T \left( \frac{\partial V}{\partial T} \right)_P}{C_P}$$

$\langle \text{例 2} \rangle$  Adiabatic Free Expansion  $\rightarrow U$  constant

$$\begin{aligned} \mu_J = \left( \frac{\partial T}{\partial V} \right)_U &= -\frac{\left( \frac{\partial U}{\partial V} \right)_T}{\left( \frac{\partial U}{\partial T} \right)_V} = -\frac{\left( \frac{\partial A}{\partial V} \right)_T + T \left( \frac{\partial S}{\partial V} \right)_T}{C_V} \\ &= -\frac{-P + T \left( \frac{\partial P}{\partial T} \right)_V}{C_V} = \frac{P}{C_V} - \frac{T\alpha}{C_V \kappa_T} = \frac{(P\kappa_T - \alpha T)}{C_V \kappa_T} \end{aligned}$$

① 如為 ideal gas,  $C_V = \frac{3}{2}R$ ,  $\alpha = \frac{1}{T}$ ,  $\kappa_T = \frac{1}{P}$ , 則  $\left( \frac{\partial T}{\partial V} \right)_U = 0$

② 如為 vdW gas, 且  $C_V$  是 constant, 因  $P = \frac{RT}{V-b} - \frac{a}{V^2}$ ,  $\left( \frac{\partial P}{\partial T} \right)_V = \frac{R}{V-b}$

$$\left( \frac{\partial T}{\partial V} \right)_U = \frac{1}{C_V} \left( P - \frac{RT}{V-b} \right) = \frac{-a}{C_V V^2}$$

$$dT = \frac{-a}{C_V V^2} dV, \Delta T = \frac{a}{C_V} \left( \frac{1}{V_2} - \frac{1}{V_1} \right), \text{ 和上一章結果一致}$$

$\langle \text{例 3} \rangle$  Reversible Adiabatic Process  $\rightarrow S$  constant

$$\left( \frac{\partial T}{\partial P} \right)_S = \frac{-\left( \frac{\partial S}{\partial P} \right)_T}{\left( \frac{\partial S}{\partial T} \right)_P} = \frac{\left( \frac{\partial V}{\partial T} \right)_P}{\frac{1}{T} C_P} = \frac{\alpha VT}{C_P}$$

$$\textcircled{1} \text{ 對 ideal gas 而言, } \alpha = 1/T, \left(\frac{\partial T}{\partial P}\right)_S = \frac{V}{C_p} = \frac{RT}{C_p P}$$

$$\frac{dT}{T} = \frac{R}{C_p} \frac{dP}{P}, \frac{T_2}{T_1} = \left(\frac{P_2}{P_1}\right)^{R/C_p}$$

$$\begin{aligned} \textcircled{2} \text{ vdW 式子因 } \alpha \text{ 不易求, 可考慮 } \left(\frac{\partial T}{\partial V}\right)_S &= \frac{-\left(\frac{\partial S}{\partial V}\right)_T}{\left(\frac{\partial S}{\partial T}\right)_V} = -\left(\frac{\partial P}{\partial T}\right)_V / C_v / T = -T \left(\frac{\partial P}{\partial T}\right)_V / C_v \\ &= \frac{-RT}{(V-b)}, \text{ 故 } \frac{dT}{T} = \frac{-dV}{V-b} \left(\frac{R}{C_v}\right), \left(\frac{T_2}{T_1}\right) = \left(\frac{V_2-b}{V_1-b}\right)^{-R/C_v} \end{aligned}$$

〈例 4〉 Isothermal Process  $\rightarrow T$  constant

$$\begin{aligned} \left(\frac{\partial U}{\partial P}\right)_T &= \left(\frac{\partial G}{\partial P}\right)_T + T \left(\frac{\partial S}{\partial P}\right)_T - \left(\frac{\partial PV}{\partial P}\right)_T = V + T \left(\frac{\partial S}{\partial P}\right)_T - V - P \left(\frac{\partial V}{\partial P}\right)_T \\ &= -T \left(\frac{\partial V}{\partial T}\right)_P + PV \kappa_T = V(\kappa_T P - \alpha T) \end{aligned}$$

$$\textcircled{1} \text{ 對 ideal gas, } \left(\frac{\partial U}{\partial P}\right)_T = 0$$

② 對 vdW gas, 複雜, 用  $\left(\frac{\partial U}{\partial V}\right)_T$  較方便

$$\left(\frac{\partial A}{\partial V}\right)_T + T \left(\frac{\partial S}{\partial V}\right)_T = -P + T \left(\frac{\partial P}{\partial T}\right)_T$$

4. 計算  $\Delta S$  之另一方法

$$\textcircled{1} \left(\frac{\partial S}{\partial P}\right)_T = -\left(\frac{\partial V}{\partial T}\right)_P \text{ ideal gas } \Rightarrow V = \frac{RT}{P} \text{ 故 } \left(\frac{\partial V}{\partial T}\right)_P = \frac{R}{P}, dS = \frac{-R}{P} dP, \Delta S = -R \ln \frac{P_2}{P_1} = R \ln \frac{V_2}{V_1}$$

$$\left(\frac{\partial S}{\partial V}\right)_T = \left(\frac{\partial P}{\partial T}\right)_V$$

$$\textcircled{2} \left(\frac{\partial S}{\partial T}\right)_V = \left(\frac{\partial S}{\partial U}\right)_V \left(\frac{\partial U}{\partial T}\right)_V = \frac{C_v}{T}, \Delta S = \int \frac{C_v}{T} dT$$

$$\textcircled{3} \left(\frac{\partial S}{\partial T}\right)_P = \frac{C_p}{T}, \Delta S = \int \frac{C_p}{T} dT$$

上一章之通式亦可由  $dS = \left(\frac{\partial S}{\partial T}\right)_V dT + \left(\frac{\partial S}{\partial V}\right)_T dV = \frac{C_v}{T} dT + \left(\frac{\partial P}{\partial T}\right)_V dV$  得到



### 4.4 Gibbs Energy Calculation

1.  $\Delta G$  之 pressure dependence:

$$dG = -SdT + VdP, \left(\frac{\partial G}{\partial P}\right)_T = V$$

故定溫下,  $\Delta G = \int_{P_1}^{P_2} VdP$

(1) ideal gas,  $dG = \frac{RT}{P} dP$ ,  $\Delta G = RT \ln \frac{P_2}{P_1}$

$G(T, P) = G^\circ(T) + RT \ln \left(\frac{P}{P^\circ}\right) = G^\circ(T) + RT \ln P$  (in bar) (用  $P/P^\circ$  較好,  $\ln$  內之參數應無單位)  
 standard state ( $P = 1 \text{ bar}$ )

☆ 如用 1atm 為 reference state, 則  $G^{\text{atm}} = G^\circ + RT \ln 1.01325 = G^\circ + 0.01316 RT$

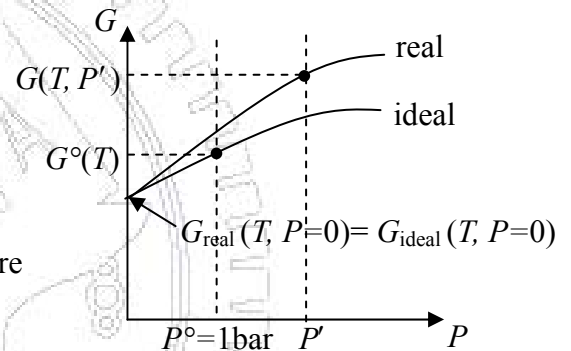
at 298 K,  $G^{\text{atm}} - G^\circ = 7.8 \text{ cal mol}^{-1}$  或  $32.6 \text{ J mol}^{-1}$ , 相差不是很大

(2) Real gas :

$G(T, P) = G^\circ(T) + RT \ln \left(\frac{f}{P^\circ}\right)$  (此即 fugacity 之定義)

ideal gas 之 fugacity 即為 pressure

- ①  $P \rightarrow 0$  時, 由 (1) 之式知  $G$  變為  $-\infty$ , 不太好
- ② 對 real gas, 可視為 "ideal" 或 "corrected" vapor pressure
- ③ 此時之 standard state 是一個 hypothetical state (如以前所述  $\Delta H^\circ$  之 standard state)



$$\begin{aligned} G_{\text{real}}(T, P') - G^\circ(T) &= RT \ln \frac{f'}{P^\circ} \\ &= G_{\text{real}}(T, P') - \lim_{P'' \rightarrow 0} [G_{\text{real}}(T, P'') - G_{\text{ideal}}(T, P'')] - G^\circ(T) \\ &= G_{\text{real}}(T, P') - G_{\text{real}}(T, P=0) - [G^\circ(T) - G_{\text{ideal}}(T, P=0)] \\ &= \int_0^{P'} V_{\text{real}} dP - \int_0^{P^\circ} \frac{RT}{P} dP \quad (\text{好像是 } P^\circ \rightarrow 0 \rightarrow P') \\ &= \int_0^{P'} V_{\text{real}} dP - \int_0^{P'} \frac{RT}{P} dP - \int_{P'}^{P^\circ} \frac{RT}{P} dP \\ &= \int_0^{P'} V_{\text{real}} dP - \int_0^{P'} \frac{RT}{P} dP - RT \ln \frac{P^\circ}{P'} \end{aligned}$$

故  $RT \ln \frac{f'}{P^\circ} + RT \ln \frac{P^\circ}{P'} = \int_0^{P'} \left( V_{\text{real}} - \frac{RT}{P} \right) dP$

$RT \ln \frac{f'}{P^\circ} = \int_0^{P'} \left( V_{\text{real}} - \frac{RT}{P} \right) dP$

ideal gas 的  $f$

$RT \ln f$  與  $RT \ln P$  之差異即為  $\int \Delta V dP$

$V_{\text{real}} - V_{\text{ideal}}$

或  $G_{\text{real}}(T, P') = \underbrace{G^\circ(T) + RT \ln \frac{P'}{P^\circ}}_{\text{ideal}} + \int_0^{P'} \left( V_{\text{real}} - \frac{RT}{P} \right) dP$

如用  $PV = RT + BP$ , 則  $V = \frac{RT}{P} + B$ , 或  $P = \frac{RT}{V - B}$

$$RT \ln \frac{f'}{P'} = \int_0^{P'} B dP = BP'$$

故  $f' = P' e^{BP'/RT}$  (常用的  $f$  與  $P$  之關係式)

(3) solid or liquid 如  $V$  幾乎不隨  $P$  而變, 則

$$G(T, P) = G^\circ(T) + V(P - P^\circ)$$

↑ standard state 即 pure substance at  $P^\circ$

## 2. $\Delta G$ 之 temperature dependence

①  $dG = -SdT + VdP$ , 故  $\left(\frac{\partial G}{\partial T}\right)_P = -S = \frac{G - H}{T}$

但  $\left(\frac{\partial \frac{G}{T}}{\partial T}\right)_P = \frac{1}{T} \left(\frac{\partial G}{\partial T}\right)_P - \frac{G}{T^2} = \frac{G - H}{T^2} - \frac{G}{T^2} = \frac{-H}{T^2}$  Gibbs-Helmholz Equation

或是  $\left(\frac{\partial \frac{G}{T}}{\partial \frac{1}{T}}\right)_P = \left(\frac{\partial \frac{G}{T}}{\partial T}\right)_P \left(\frac{\partial T}{\partial \frac{1}{T}}\right)_P = -T^2 \left(\frac{\partial \frac{G}{T}}{\partial T}\right)_P = H$

對於化學反應,  $\left(\frac{\partial \frac{\Delta G}{T}}{\partial \frac{1}{T}}\right)_P = \Delta H$  或  $\left(\frac{\partial \frac{\Delta G}{T}}{\partial T}\right)_P = \frac{-\Delta H}{T^2}$

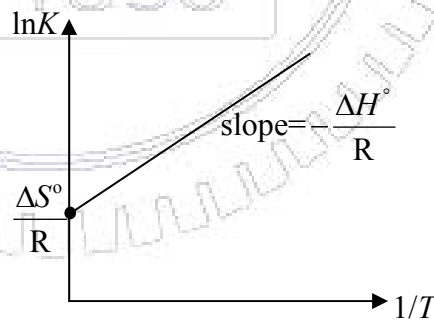
即:  $G$  與  $H$  並不是毫不相關的, 粗略講即是因  $\Delta S$  決定  $\Delta G$  之 temperature dependence, 使得  $\Delta H$  也和  $\Delta G$  之 temperature dependence 相關

以後會教到  $\Delta G^\circ = -RT \ln K$

故  $\left(\frac{\partial \ln K}{\partial \frac{1}{T}}\right) = -\frac{\Delta H^\circ}{R}$

$\ln K = -\frac{\Delta H^\circ}{RT} + \text{intercept}$

$= -\frac{\Delta G^\circ}{RT} = -\frac{\Delta H^\circ}{RT} + \frac{T\Delta S^\circ}{RT}$



② 如  $C_p = a + bT + cT^{-2}$

則  $\Delta H = \int C_p dT = \int a + bT + cT^{-2} dT = a(T - T_0) + \frac{b}{2}(T^2 - T_0^2) - c\left(\frac{1}{T} - \frac{1}{T_0}\right)$

$= \Delta H_0 + aT + \frac{b}{2}T^2 - cT^{-1}$

其中  $\Delta H_0 = -\left(aT_0 + \frac{b}{2}T_0^2 - c\frac{1}{T_0}\right)$

$$\text{故 } \frac{\Delta H}{T^2} = \frac{\Delta H_0}{T^2} + \frac{a}{T} + \frac{b}{2} - \frac{C}{T^3}$$

$$-\frac{\Delta G}{T} = \int \frac{\Delta H}{T^2} dT = \frac{-\Delta H_0}{T} + a \ln T + \frac{b}{2} T + \frac{C}{2T^2} + I, I \text{ 是 } \frac{\Delta H_0}{T_0} - a \ln T_0 - \frac{b}{2} T_0 - \frac{C}{2T_0^2}$$

$$\Delta G = \Delta H_0 - aT \ln T - \frac{b}{2} T^2 - \frac{C}{2} \frac{1}{T} - IT$$

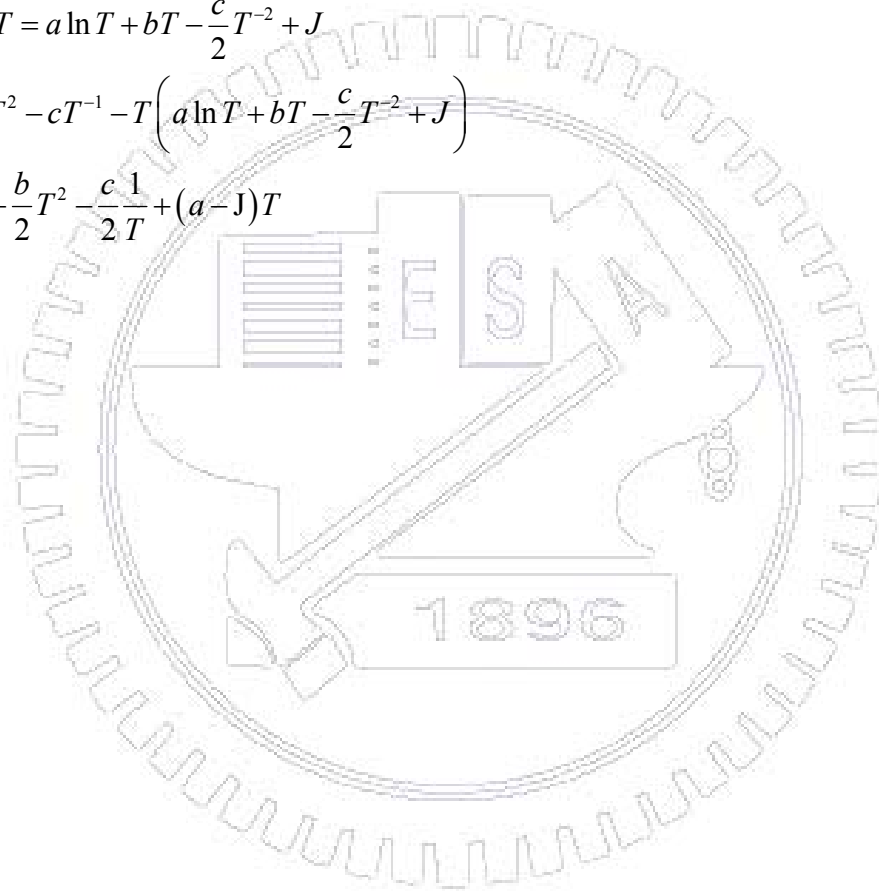
$$\text{欲知 } \Delta G(T), \text{ 可由 } \begin{cases} \text{某一 } T \text{ 之 } \Delta H \\ C_p(T) \\ \text{某一 } T \text{ 之 } \Delta G \end{cases} \quad \text{或} \quad \begin{cases} C_p(T) \\ \text{某一 } T \text{ 之 } \Delta S \\ \text{某一 } T \text{ 之 } \Delta G \text{ 或 } \Delta H \end{cases}$$

另法：用  $\Delta S = \int \frac{C_p}{T} dT$ ，再用  $\Delta G = \Delta H - T\Delta S$  更快

$$\Delta S = \int \frac{a}{T} + b + cT^{-3} dT = a \ln T + bT - \frac{c}{2} T^{-2} + J$$

$$\Delta G = \Delta H_0 + aT + \frac{b}{2} T^2 - cT^{-1} - T \left( a \ln T + bT - \frac{c}{2} T^{-2} + J \right)$$

$$= \Delta H_0 - aT \ln T - \frac{b}{2} T^2 - \frac{c}{2} \frac{1}{T} + (a - J)T$$



### 4.5 Multicomponent System

single component system-由  $P, V, T$  中 2 個 variable 描述  
 c-component system-  $c+1$  for single phase (不含總 mole 數)  
 (c-p+2 for p-phase, 以後說明)

課本用  $c+2$  是包含總 mole 數

未必就等於 species 之數目, 如:  $2\text{NO}_2 = \text{N}_2\text{O}_4$  平衡, 只能算 1 個 component

原來  $G(P, T) \rightarrow G(P, T, n_1, n_2, \dots, n_c)$ , 其中有一個  $n_j$  是 redundant (多餘的)

$$dG = \left(\frac{\partial G}{\partial T}\right)_{P, n} dT + \left(\frac{\partial G}{\partial P}\right)_{T, n} dP + \sum_{i=1}^c \left(\frac{\partial G}{\partial n_i}\right)_{T, P, n'} dn_i \quad (n \text{ 表全部之 } n_j; n' \text{ 表除了 } n_i \text{ 外之 } n_j)$$

$$= -SdT + VdP + \sum_{i=1}^c \mu_i dn_i$$

同理  $dA = -SdT - PdV + \sum_{i=1}^c \left(\frac{\partial A}{\partial n_i}\right)_{T, V, n'} dn_i \dots = \left(\frac{\partial A}{\partial n_i}\right)_{T, V, n'} = \left(\frac{\partial U}{\partial n_i}\right)_{S, V, n} = \left(\frac{\partial H}{\partial n_i}\right)_{S, P, n'}$

$\mu_i = \left(\frac{\partial G}{\partial n_i}\right)_{T, P, n'}$  chemical potential

Partial Molar Quantity:  $\bar{Y}_i = \left(\frac{\partial Y}{\partial n_i}\right)_{T, P, n'}$

extensive  
↑  
intensive

通常  $T, P$  hold constant 者才算是, 故上面 3 個不是

① 以前之式子均能適用, 只要  $G \rightarrow \mu_i, H, U, A, S, V \rightarrow \bar{H}_i, \bar{U}_i, \dots$  etc.

② 對於 1-component system,  $\bar{Y}_i = \bar{Y} = Y/n$ , 即  $Y = n\bar{Y}_i$

③ 對於 c-component system,  $Y = \sum_{i=1}^c n_i \bar{Y}_i$

或  $\bar{Y} = \frac{1}{n} Y = \sum_{i=1}^c \frac{n_i}{n} \bar{Y}_i = \sum_{i=1}^c x_i \bar{Y}_i = \bar{Y}$ , 其中  $\bar{Y}$  為總 mole 數為 1 之量,

$x_i$  為  $i$ th component 之 mole fraction

④  $\bar{Y}_i$  是 concentration dependent

### 4.6 Euler's Theorem and the Gibbs-Duhem Relation

1. 如  $f(\lambda x_1, \lambda x_2, \dots, \lambda x_c) = \lambda^k f(x_1, x_2, \dots, x_c)$

f 即為 homogeneous function of degree  $k$ , 令  $k=1$  即和上式相同

$$\text{Euler's Theorem: } kf = \sum_{i=1}^c x_i \left( \frac{\partial f}{\partial x_i} \right)_{x'}$$

$$\left( \text{證明：兩邊對 } \lambda \text{ 微分, } \sum_i \left( \frac{\partial f}{\partial \lambda x_i} \right)_{x'} \left( \frac{\partial \lambda x_i}{\partial \lambda} \right)_{x'} = k \lambda^{k-1} f, \text{ 再令 } \lambda = 1 \right)$$

↓  
=  $x_i$

### 2. Gibbs-Duhem Relation

$$\text{因 } Y = \sum_{i=1}^c n_i \bar{Y}_i$$

$$dY = \sum_i n_i d\bar{Y}_i + \sum_i \bar{Y}_i dn_i$$

$$\text{又 } dY = \left( \frac{\partial Y}{\partial T} \right)_{P, n} dT + \left( \frac{\partial Y}{\partial P} \right)_{T, n} dP + \sum_{i=1}^c \bar{Y}_i dn_i$$

$$\text{故 } \boxed{\sum_i n_i d\bar{Y}_i = \left( \frac{\partial Y}{\partial T} \right)_{P, n} dT + \left( \frac{\partial Y}{\partial P} \right)_{T, n} dP}$$

generalized Gibbs-Duhem relation

$$\boxed{\sum_i n_i d\bar{Y}_i = 0} \quad \text{at constant } T, P$$

如  $Y$  為  $G$ , 即  $\sum_i n_i d\mu_i = 0$

Gibbs-Duhem relation

(1) 以 volume 為例：用 binary system (含  $n_A$  mole 的 A 及  $n_B$  mole 的 B)

$$\bar{V}_A = \left( \frac{\partial V}{\partial n_A} \right)_{T, P, n_B}, \quad \bar{V}_B = \left( \frac{\partial V}{\partial n_B} \right)_{T, P, n_A}$$

$$V = n_A \bar{V}_A + n_B \bar{V}_B$$

而 Gibbs Duhem equation  $\Rightarrow$  ①  $\frac{d\bar{V}_A}{d\bar{V}_B} = \frac{-n_B}{n_A}$  即  $\bar{V}_A$  及  $\bar{V}_B$  是相關的

$$\text{② } dV = \bar{V}_A dn_A + \bar{V}_B dn_B$$

①  $\Delta V_{\text{mix}} = V - (n_A V_A^* + n_B V_B^*)$ , 其中 g 表 pure substance

$$= (n_A \bar{V}_A + n_B \bar{V}_B) - n_A \bar{V}_A^* - n_B \bar{V}_B^* = \boxed{n_A (\bar{V}_A - \bar{V}_A^*) + n_B (\bar{V}_B - \bar{V}_B^*)}$$

適用於任何 state function, 如:  $G, H$

②  $\bar{V}_A$  與  $\bar{V}_B$  之關係

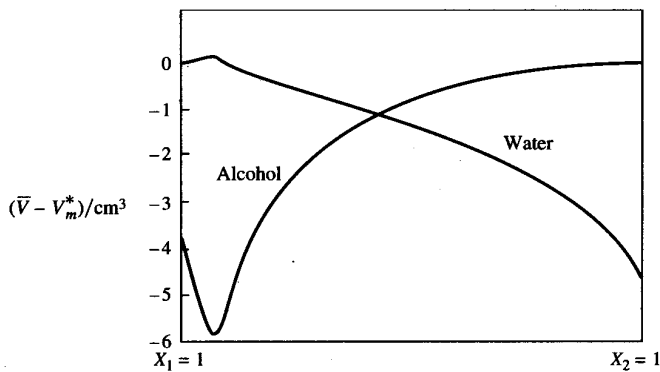
$$d\bar{V}_A = \frac{-n_B}{n_A} d\bar{V}_B = \frac{x_B}{x_B - 1} d\bar{V}_B, \text{ 因 } x_B = \frac{n_B}{n_A + n_B}, 1 - x_B = \frac{n_A}{n_A + n_B}$$

故  $\int d\bar{V}_A = \int \frac{x_B}{x_B - 1} d\bar{V}_B = -\int \frac{x_B}{1 - x_B} d\bar{V}_B$  (1) 由其中之一  $\bar{V}_i$  的變化即已決定另一  $\bar{V}_i$  之變化

(2) 一個有 max., 另一個即有 min.

(3) 與軸之交點即為  $V_A^*$  及  $V_B^*$

(4) 在  $x = 0.5$  時, slope 等值異號



以  $H_2O/C_2H_5OH$  為例 (圖 a,  $H_2O$  為 1,  $C_2H_5OH$  為 2)

For  $C_2H_5OH$ , min. 在  $x_2 = 0.064$

即  $\frac{0.064 \times 46}{0.064 \times 46 + 0.936 \times 18} = 15\% \text{ by weight}$

(a)

③  $\bar{V}_i$  可以是負值 (即: B 加入使總體積變小)

如:  $MgSO_4$ , 由於 electrostriction 使水結構被破壞

(2) Free energy of mixing :

用氣體 mixing 來說明,  $G = G^o + RT \ln \frac{P}{P^o} \rightarrow \mu = \mu^o + RT \ln \frac{P}{P^o}$

$$\begin{cases} \text{混合前 } x_1 \mu_1^o + x_2 \mu_2^o \\ \text{混合後 } x_1 (\mu_1^o + RT \ln x_1) + x_2 (\mu_2^o + RT \ln x_2) = 0 \end{cases}$$

$$\frac{P_f}{P_i} = \frac{n_1}{n_1 + n_2}$$

$$\begin{aligned} \Delta G &= x_1 RT \ln x_1 + x_2 RT \ln x_2 \\ &= RT \sum_i x_i \ln x_i \end{aligned}$$

$$\Delta S = - \left( \frac{\partial \Delta G}{\partial T} \right)_p = -R \sum_i x_i \ln x_i$$

$$\Delta H = 0$$

另一作法:

定溫  $\Delta G = \Delta H - T\Delta S = -T\Delta S$

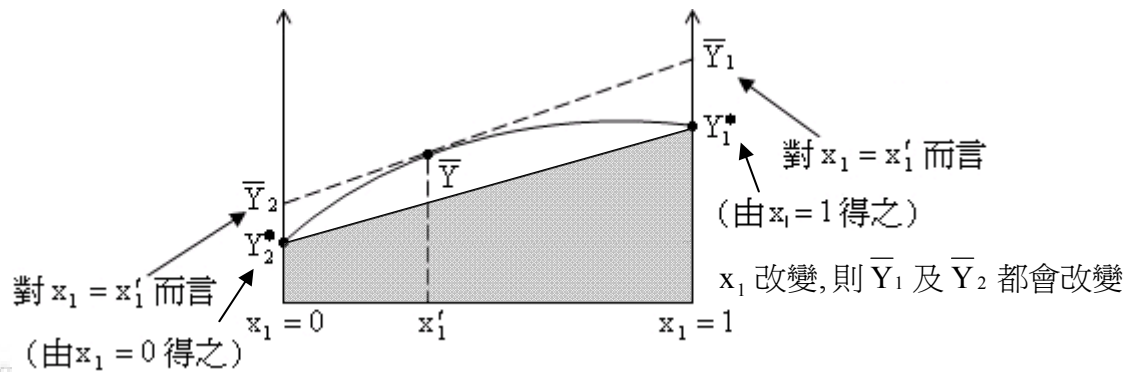
3. Determination of Partial Molar Quantities (Experimental)

① Method of intercepts

$$\bar{Y} = x_1 \bar{Y}_1 + x_2 \bar{Y}_2 = (\bar{Y}_1 - \bar{Y}_2)x_1 + \bar{Y}_2 \quad (\text{因 } x_2 = 1 - x_1)$$

$$\begin{aligned} \text{又 } \left( \frac{\partial \bar{Y}}{\partial x_1} \right)_{T,P} &= \bar{Y}_1 - \bar{Y}_2 + x_1 \frac{\partial \bar{Y}_1}{\partial x_1} - x_1 \frac{\partial \bar{Y}_2}{\partial x_1} + \frac{\partial \bar{Y}_2}{\partial x_1} \\ &= \bar{Y}_1 - \bar{Y}_2 + x_1 \frac{\partial \bar{Y}_1}{\partial x_1} + x_2 \frac{\partial \bar{Y}_2}{\partial x_1} = \bar{Y}_1 - \bar{Y}_2 \\ &= 0 \quad \text{from Gibbs-Duhem relation} \end{aligned} \quad (\text{注意: } Y_i \text{ 是 concentration dependent})$$

$$\text{故 } \bar{Y} = \left( \frac{\partial \bar{Y}}{\partial x_1} \right)_{T,P} x_1 + \bar{Y}_2$$



如要準確, 則可用  $\Delta \bar{Y}_{\text{mix}}$  作圖 (即: 把上圖中之灰色部分切掉, 拉平)

參考課本 Figure 4.3

$$\Delta \bar{Y}_{\text{mix}} = \bar{Y} - x_1 \bar{Y}_1 - x_2 \bar{Y}_2$$

$$= \bar{Y} - \left[ \bar{Y}_2 + x_1 (\bar{Y}_1 - \bar{Y}_2) \right]$$

$$x_1 = 0 : \text{左截距} = \bar{Y} - \bar{Y}_2 = \bar{Y}_2 - \bar{Y}_2$$

$$x_1 = 1 : \text{右截距} = \bar{Y} - \bar{Y}_1 = \bar{Y}_1 - \bar{Y}_1$$

※注意※

左圖和上圖是不同的系統, 並非由上圖可得到左圖。

Apparent molar quantity method (以 volume 為例)

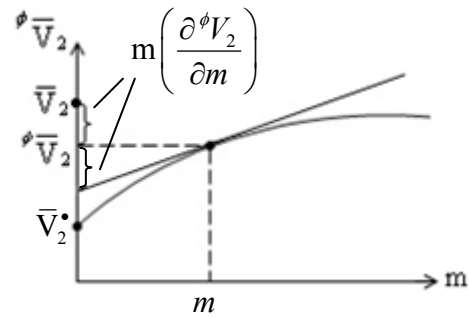
$$\text{Apparent molar volume } \phi \bar{V}_2 = \frac{V - n_1 \bar{V}_1}{n_2}$$

即加入 "2" (solute) 使得總 volume 之增加量

如  $n_1 = \frac{1000}{M_1}$  , 則  $n_2 = m$

$$V = m \phi \bar{V}_2 + \frac{1000}{M_1} \bar{V}_1$$

$$\bar{V}_2 = \left( \frac{\partial V}{\partial m} \right) = \phi \bar{V}_2 + m \left( \frac{\partial \phi \bar{V}_2}{\partial m} \right)$$



即：把  $\phi \bar{V}_2$  值再加上截距與  $\phi \bar{V}_2$  之差值可得  $\bar{V}_2$

